

**WEST**[Help](#)[Logout](#)[Interrupt](#)[Main Menu](#)[Search Form](#)[Posting Counts](#)[Show S Numbers](#)[Edit S Numbers](#)[Preferences](#)**Search Results -**

Terms	Documents
16 and membrane	77

Database:

US Patents Full-Text Database	▲
JPO Abstracts Database	
EPO Abstracts Database	
Derwent World Patents Index	
IBM Technical Disclosure Bulletins	▼

Refine Search:

16 and membrane

[Clear](#)**Search History**

Today's Date: 3/1/2001

<u>DB Name</u>	<u>Query</u>	<u>Hit Count</u>	<u>Set Name</u>
USPT	16 and membrane	77	<u>L8</u>
USPT	14 and resin	0	<u>L7</u>
USPT	13 and ion exchange	153	<u>L6</u>
USPT	13 and ion exchange	153	<u>L5</u>
USPT	13 and ion exchange	0	<u>L4</u>
USPT	electrical same regeneration	1167	<u>L3</u>
USPT	ion exchange and regenerated and electrically	1	<u>L2</u>
USPT	ion exchange and regenerated and electrically	1	<u>L1</u>

**WEST**

Help

Logout

Interrupt

Main Menu

Search Form

Posting Counts

Show S Numbers

Edit S Numbers

Preferences

**Search Results -**

Terms	Documents
114 and reverse osmosis	57

Database: 

US Patents Full-Text Database	▲
JPO Abstracts Database	
EPO Abstracts Database	
Derwent World Patents Index	
IBM Technical Disclosure Bulletins	▼

Refine Search:

Clear

**Search History**

Today's Date: 3/1/2001

<u>DB Name</u>	<u>Query</u>	<u>Hit Count</u>	<u>Set Name</u>
USPT	114 and reverse osmosis	57	<u>L15</u>
USPT	oxidizing agent and electrodialysis	158	<u>L14</u>
USPT	210/750 and 18	0	<u>L13</u>
USPT	210/759 and 18	0	<u>L12</u>
USPT	110 and 18	0	<u>L11</u>
USPT	210/758	1100	<u>L10</u>
USPT	210/758-759	4	<u>L9</u>
USPT	16 and membrane	77	<u>L8</u>
USPT	14 and resin	0	<u>L7</u>
USPT	13 and ion exchange	153	<u>L6</u>
USPT	13 and ion exchange	153	<u>L5</u>
USPT	13 and ion exchange	0	<u>L4</u>
USPT	electrical same regeneration	1167	<u>L3</u>
USPT	ion exchange and regenerated and electrically	1	<u>L2</u>
USPT	ion exchange and regenerated and electrically	1	<u>L1</u>

**WEST**

Generate Collection

L8: Entry 14 of 77

File: USPT

Sep 22, 1998

DOCUMENT-IDENTIFIER: US 5811012 A

TITLE: Deionized water or high purity water producing method and apparatus

ABPR:

A deionized or high purity water producing method is describing wherein ions and non-ionic substances are removed. The method includes pretreating feed water to remove suspended non-ionic substances, containing the pretreated water with first and second ion exchange resins that include a boron selective ion exchange resin, and stratifying or mixing together the first and second resins within an ion exchange column. The boron selective ion exchange resin is included to remove boron ions contained in the pretreated water.

BSPR:

In FIG. 17, 1 is a pretreatment unit for removing suspended solids and some of the organic matter from feed water such for example as industrial water. Pretreated water, after passing through a filtered water tank 2, is sent to a two bed ion exchange deionization system (two-bed with a degasifier type) 3 comprising a cation exchange resin column (K column) 31, a decarbonating column 32 and an anion exchange resin column (A column) 33 where ionic impurities are removed. 4 is a demineralized water storage tank for storing treated water after removal of these ionic impurities.

BSPR:

5 is an RO (Reverse Osmosis) apparatus comprising a reverse osmosis membrane which removes impurities such as residual inorganic ions, organic matter and minute particles in the treated water from which most of the impurity ions have been removed by the two bed ion exchange deionized system 3. 6 is a tank for storing RO treated water.

BSPR:

From the effluent of this cartridge polisher 11, minute particles are removed by an ultrafiltration apparatus 12 comprising an ultrafiltration membrane, and the resulting high purity water is supplied to points of use 13 where it is used.

BSPR:

In view of the aforesaid problems inherent to the conventional ion exchange deionization technology, this invention was conceived to provide a method and apparatus for producing deionized or high purity water having reduced boron concentrations.

BSPR:

It is another aim of this invention to provide a method and apparatus for producing deionized or high purity water wherein the boron concentration is constantly maintained at low levels without the need to increase the number of regeneration cycles of a regenerating ion exchanger, or the frequency of replacing the ion exchange resins in a non-regenerating ion exchanger.

BSPR:

According to the first invention, in a method for producing deionized or high purity water comprising pretreatment to remove suspended solids, and downstream purification treatment to remove ionic and non-ionic substances from the pretreated water, the pretreated water is brought into contact with a boron selective ion exchange resin to remove boron at some stage of the downstream purification treatment.

BSPR:

The boron selective ion exchange resin used in the first invention may be any ion exchange resin that selectively removes boron, typical examples being AMBERLITE (trade name: Rohm and Haas Company) IRA-743T and DIALON CRB02 (Mitsubishi Kasei) containing polyhydric alcohol groups as functional groups. According to this invention, the use of these boron selective ion exchange resins is sine qua non. If conventional strongly basic anion exchange resins which were previously considered to have excellent boron adsorption capacities and high exchange capacities are used instead, large amounts of boron are unexpectedly leaked at an early stage as described hereinbefore, so the object of this invention cannot be achieved.

BSPR:

The term "pretreatment" referred to hereinabove may be any treatment that comprises coagulation/sedimentation, filtration, in-line coagulation/filtration, activated carbon adsorption, membrane turbidity removal, and so forth.

BSPR:

The term "purification treatment" referred to hereinabove may be any treatment that comprises ion exchange, reverse osmosis, electrical regeneration ion exchange, and so forth.

BSPR:

The phrase "pretreated water is brought into contact with a boron selective ion exchange resin" refers to the process wherein pretreated water is passed through an ion exchange column packed with a boron selective ion exchange resin, although other ion exchange resins may be mixed with or arranged in layers with this boron selective resin in the column.

BSPR:

The second invention relates to the deionized water or high purity water producing apparatus used to implement the aforesaid method. This apparatus comprises a pretreatment unit comprising turbidity removing means to remove suspended solids in the feed water, and purification treatment section comprising deionization and membrane separation means to remove ionic and non-ionic substances from the pretreated water, with an ion exchange column containing a boron selective ion exchange resin being installed as a boron ion removing means in at least one position in the water treatment system between the outlet of the pretreatment unit and the outlet of the purification treatment section.

BSPR:

The turbidity removing means in the pretreatment unit may be those for coagulation/sedimentation, filtration, in-line coagulation/filtration, activated carbon adsorption, membrane turbidity removal and so forth that perform the pretreatment of the first invention.

BSPR:

As deionizing and membrane separation means for removing ionic and non-ionic substances in the purification treatment section, the ion exchanger, electrical regeneration ion exchanger, reverse osmosis membrane and so forth which are the embodiments of the methods of the first invention may be used, but the purification treatment section comprising a primary deionized water production system for obtaining primary deionized water from water in the pretreatment unit equipped with a membrane separation means, a tank for storing this primary deionized water, and a secondary deionized water production system equipped with an ion exchange means, a membrane treatment means and so forth for obtaining high purity water from the primary deionized water in its tank, as defined in claim 3, is particularly to be preferred. The primary deionized water production system may comprise other means such as decarbonating and degassing units. Further, the second deionized water production system may comprise means such as an ultraviolet oxidation apparatus.

BSPR:

In the high purity water producing apparatus comprising the primary and secondary deionized water production systems, in general, high purity water is continually recirculated by returning excess high purity water to the primary deionized water tank via a high purity water recirculation pipe while high

purity water is used at points of use, or even when it is not used. This recirculation line and the secondary deionized water production system forms a closed loop with the secondary deionized water production system consisting of, for example, an ultraviolet oxidation apparatus, a cartridge ion exchange polisher and an ultrafiltration membrane apparatus. The same recirculation arrangement is also adopted to advantage in the present invention, because if the operation of the high purity water production system is stopped while high purity water is not being used at points of use, the water stagnates in the pipes and treatment systems. This leads to proliferation of bacteria, release of ions and organic substances albeit in small amounts, and deterioration of the quality of high purity water. Furthermore, minute particles may be leaked from the materials used for the system due to shocks created at the time of stopping or re-starting the system.

BSPR:

The ion exchange column containing the boron selective ion exchange resin may be installed in the middle of the flowpath taken by the pretreated water flowing out of the pretreatment unit, between pieces of equipment in the purification treatment section, or in the deionized water or high purity water flowpath from the purification treatment section (actually, at a point preceding the last membrane treatment apparatus in the secondary deionized water production system). The ion exchange column may be packed with a boron selective ion exchange resin alone, with a mixture of another resin with the boron selective resin, or with another resin or resins and the boron selective resin arranged in layers. These columns may be provided at one, two or more positions, however it is often preferable to provide one as a regenerating type in any position between the anion (A) column of the two bed ion exchange deionization system and the regenerating type mixed bed ion exchanger in the primary deionized water production system, or as a non-regenerating type in the deionized water flowpath from the primary to the secondary deionized water production system. Further, in addition to providing an ion exchange column containing a boron selective ion exchange resin in the main flowpath of the deionized water or high purity water production system, a column may be provided also in the middle of the recirculation line (e.g. the line that returns high purity water to the primary deionized water tank).

BSPR:

The ion exchange column containing the boron selective resin may contain this resin alone, or mixed with another resin, e.g. a strongly acidic cation resin or strongly basic anion resin, alternatively these resins may be arranged in layers. In this context, the term "layers" refers to the situation where two or more resins are packed in one column, the two or more resins being used not as a mixture but as layers when water is passed through them. Typically, a cation exchange resin may be arranged downstream of the boron selective ion exchange resin in one column, or an anion exchange resin may be arranged upstream of the boron selective ion exchange resin in one column. In these cases, the boron selective ion exchange resin can be regenerated by using a regenerating means that passes an acidic aqueous solution through a column containing a layer of a cation exchange resin, and a regenerating means that passes an alkaline aqueous solution through a column containing a layer of an anion exchange resin. The boron selective ion exchange resin can be regenerated by either acid or alkali.

BSPR:

The term "mixed" refers to the situation where two or more resins are packed in one column, the two or more resins being used in admixture with one another. A typical example is a regenerative type mixed bed ion exchanger wherein a boron selective ion exchange resin, cation exchange resin and anion exchange resin are mixed together. In this mixed bed ion exchanger, if a boron selective resin having a lower specific gravity than the anion exchange resin is used, a separation can be made in the order of, from the bottom, cationic resin--anionic resin--boron selective resin, so an ordinary regeneration arrangement for the mixed bed ion exchanger can be employed using both an acidic aqueous solution and an alkaline aqueous solution as regenerating agents.

BSPR:

The ion exchange column containing a boron selective ion exchange resin may also be a non-regenerative type, in which case it is often preferable to

install it downstream of the primary deionized water production system in the deionized water or high purity water treatment apparatus comprising the aforesaid primary--secondary systems.

BSPR:

In view of the leakage of organic matter from these resins, at least one, and preferably both of, an ultraviolet oxidation apparatus and a reverse osmosis membrane apparatus may be installed downstream of the ion exchange column containing the boron selective ion exchange resin.

BSPR:

As devices and equipment such as ion exchangers and membrane separators that comprise the deionized water or high purity water producing apparatus of this invention, those known in the art may be used without modification, and the basic system of a conventional deionized water or high purity water production apparatus may also be applied to this invention without modification.

BSPR:

In this deionized water or high purity water producing apparatus provided with an ion exchange column containing a boron selective ion exchange resin, either a fixed throughput endpoint operation or an operation wherein the leakage of boron is monitored may be adopted for both the regenerating and non-regenerating types of boron selective resin column. If the leakage of boron is monitored, the boron meter may be an instrument wherein a boron derivative is generated using a chronotropic acid, and the intensity of fluorescence of this derivative is measured by a fluorescence photometer, or alternatively, the measurement may be performed by an ICP-MS analyzer that measures boron directly with high sensitivity. These boron meters may be installed "in-line" at the place of measurement, or alternatively these may be installed externally from the deionized water or high purity water producing apparatus and the boron concentration measured externally. The boron monitoring may be done by measuring and observing the boron concentration in the effluent of the ion exchange column containing a boron selective ion exchange resin, and replacing the resin or regenerating it when the boron concentration reaches a predetermined value. This predetermined value may be determined according to the purpose of using deionized or high purity water, taking into account the allowable upper limit of boron concentration in the deionized water or high purity water.

BSPR:

A plurality of these ion exchange columns containing a boron selective ion exchange resin may be connected in series, the first column being regenerated and transferred to the last stage when the resin in the first column has reached a fixed throughput (or when the boron concentration in the treated water from the first column has reached the predetermined value). Alternatively, a merry-go-around system can be adopted. In this system, the first column is removed and a new column, which has new or regenerated resin, is connected to the last column. Such a system may be easily operated by switching pipes and valves.

BSPR:

According to this invention, by bringing pretreated water containing boron into contact with a boron selective ion exchange resin, i.e. an anion exchange resin into which polyhydric alcohol has been introduced as functional groups, boron can be selectively and definitively eliminated. This is the first time that it has been possible to produce deionized or high purity water, wherein boron has been reduced to extremely minute amounts, on an industrial scale.

BSPL:

This leakage of boron (i.e., the fact that the boron concentration in the high purity water was not so low) was quite unexpected. In other words, in the aforesaid conventional high purity water producing system, the two bed ion exchange deionization system 3, RO apparatus 5, regenerative type mixed bed ion exchanger 8 and cartridge polisher 11 seems to contribute to removing boron, and it is therefore unexpected that boron cannot be sufficiently removed while going through the said conventional high purity water producing system. In order to make a more detailed study of this phenomenon of higher concentrations of boron in the high purity water, the inventors continuously monitored the boron concentration in the high purity water produced by the

conventional high purity water producing system for 30 days at points of use 13 as shown in FIG. 17. It was found not only that boron was not sufficiently removed, but also that the boron concentration varied with time as shown in FIG. 16. Further, when the boron concentration was measured in the effluent of the two bed ion exchange deionization system on the condition that the ion exchangers were regenerated after every 5 days of fixed throughput endpoint operation (the exhaustion cycle was stopped to a 5-day fixed throughput endpoint before the leakage of silica or chloride ion started), it was found that whereas the electric conductivity of the treated water was maintained at a low level as shown in FIG. 15, boron leaked at a very early stage of the exhaustion cycle. Much the same phenomenon (boron ion leakage) was observed in the regenerative mixed bed ion exchanger and cartridge polisher which were located downstream of the two bed ion exchange deionization system.

DRPR:

FIG. 2 is a diagram showing the variation of boron concentration in the effluent of a two bed ion exchange system according to Example 1 and Comparative Example 1.

DRPR:

FIG. 7 is a diagram showing the variation of boron concentration in the effluent of an ion exchange column according to Embodiment 5 and Comparative Example 2.

DRPR:

FIG. 15 is a diagram showing the variation with time of boron concentration in the effluent of a two bed ion exchange system in a conventional high purity water producing apparatus.

DEPR:

FIG. 1 is a block diagram showing the essential features of the construction of a high purity water producing apparatus according to Example 1 of this invention. In the figure, 1 is a pretreatment unit for removing some of the suspended solids and organic matter in feed water such as industrial water. The water from this pretreatment is passed through a filtered water tank, (not shown), and is sent to a two bed ion exchange deionization system 3 forming a deionizer where it passes successively through a cation exchange column (K column) 311, decarbonating column 32 and anion exchange resin column (A column) 33 in order to remove ionic impurities.

DEPR:

It is an essential feature of this example that the cation exchange column (K column) 311 of the aforesaid two bed ion exchange deionization system 3, comprises an upstream layer (upper part of column) of AMBERLITE IRA-743T (Rohm and Haas Company), which is a boron selective ion exchange resin, and a downstream layer (lower part of column) of AMBERLITE IR-124 (Rohm and Haas Company), which is a strongly acidic cation exchange resin. The features and functions of this high purity water producing apparatus will now be described.

DEPR:

5 is an RO apparatus comprising a reverse osmosis membrane for removing impurities such as inorganic ions, organic matter and fine particles in the treated water from which a major portion of impurity ions has already been removed by the aforesaid two bed ion exchange deionization system 3.

DEPR:

From the effluent of this cartridge polisher 11, fine particles are removed by an ultrafiltration apparatus 12 comprising an ultrafiltration membrane so as to produce high purity water which is then supplied to points of use.

DEPR:

Apart from the cation exchange resin column 311 (K column) of the two bed ion exchange deionization system 3, the high purity water producing apparatus having the aforesaid features has much the same basic construction as the conventional high purity water producing apparatus shown in FIG. 17.

DEPR:

It is another essential feature of this example that, in the aforesaid cation

exchange resin column 311 (K column), AMBERLITE IRA-743T, which is a boron selective ion exchange resin having N-methyl-glucamine as functional groups, and AMBERLITE IR-124, are packed in layers in the column with the former resin situated above the latter resin (in this example, the volume ratio of the two resins is Amberlite IRA-743T/Amberlite IR-124 2.5/4.0). The reason for situating the boron selective resin upstream in the column is that effluent from a cation exchange resin is generally acidic with a pH of 2 or less, and if Amberlite IRA-743T were located downstream of Amberlite IR-124, the boron adsorption performance of IRA-743T would not be fully utilized. The K column may alternatively consists of a separate column packed with AMBERLITE IR-124 alone, preceded by a column packed with Amberlite IRA-743T.

DEPR:

Due to the aforesaid system scheme, boron can be selectively removed by the boron selective ion exchange resin (Amberlite IRA-743T) from pretreated water containing large amounts of other coexisting ions. The remaining coexisting ions are basically removed by the deionization function of the aforesaid two bed ion exchange deionization system 3 having a conventional structure. In the high purity water producing apparatus of this example, therefore, as boron in the pretreated water is selectively removed by the boron selective resin (Amberlite IRA-743T), passage of boron to the downstream two bed ion exchange system 3 is reduced, and leakage of boron is prevented over a long period of time without shortening the regeneration cycle time of the two bed ion exchange deionization system 3.

DEPR:

Using the aforesaid apparatus scheme, high purity water was produced under the following conditions, and the boron concentration of the effluent from the two bed ion exchange deionization system 3 was measured by an ICP-MS analyzer. The results are shown in FIG. 2.

DEPR:

Another feature of this example is the regeneration of the boron selective ion exchange resin Amberlite IRA-743T by an acid aqueous solution. The boron selective resin is generally present in its hydroxyl form, therefore in the regenerating method commonly employed, after adsorbed boron has been eluted with an acid solution, the resin is restored to its hydroxyl ion form with an aqueous solution of an alkali such as sodium hydroxide. After passing a hydrochloric acid solution through the column, therefore, regeneration is performed by passing an alkaline aqueous solution through Amberlite IRA-743T.

DEPR:

High purity water was produced using the same apparatus and conditions as those of Example 1, excepting that instead of the K column 311 of the two bed ion exchange system 3 of Example 1, an ion exchange column packed only with AMBERLITE IR-124 was used. The boron concentration of the effluent of the ion exchange deionization system 3 was measured by an ICP-MS analyzer, and the results are shown in FIG. 2 together with the results obtained from Example 1.

DEPR:

In this example shown in FIG. 3, the K column of the two bed ion exchange deionization system 3 of Example 1 was replaced with a K column 31 packed only with AMBERLITE IR-124. The A column 331 was packed with a layer of AMBERLITE IRA-743T, the aforesaid boron selective ion exchange resin, situated downstream (upper part of column) and a layer of AMBERLITE IRA-402BL situated upstream (lower part of column) (in this example, the volume ratio Amberlite IRA-743T/Amberlite IRA-402BL was 1/4). In the A column 331, influent water is passed upflow. The reason why the boron selective resin is situated downstream in the column is that the water upstream of the AMBERLITE IRA-402BL is acidic soft water and its pH is generally 2 or less. Although the boron adsorption capacity of AMBERLITE IRA-743T cannot be fully utilized under these conditions, the water treated by Amberlite IRA-402BL is neutral or slightly alkaline, so the boron adsorption capacity can then be fully exploited. The remaining system features of Example 2 are the same as those of Example 1.

DEPR:

High purity water was produced using the apparatus having the scheme shown in FIG. 3 and under the same conditions as those of Example 1, except that the K



column 31 and the A column 331 were charged with the resins as described below. The boron concentration of the effluent of the two bed ion exchange deionization system 3 was measured using a ICP-MS analyzer. The results for boron concentration were the same as those of Example 1 shown in FIG. 2.

## DEPR:

Regeneration of the resins charged in the A column 331 was effected by passing an alkaline aqueous solution through Amberlite IRA-402BL and Amberlite IRA-743T. Since an alkaline aqueous solution was used as the regenerant, the original ion exchange capacity of the boron selective resin (Amberlite IRA-743T) was restored, hence the quantity of the ion exchange resin required was reduced compared to the case of Example 1.

## DEPR:

In this example shown in FIG. 4, the apparatus has much the same basic treatment scheme as the conventional high purity water producing apparatus shown in FIG. 17 (where the K column 311 of FIG. 1 has been replaced by the K column 31 packed only with an ordinary cation exchange resin), and an ion exchange column 300 packed only with AMBERLITE IRA-743T is provided between the A column 33 of the two bed ion exchange deionization system 3 and the RO apparatus 5. This is equivalent to the case where the A column 331 of Example 2 is a separate column packed with AMBERLITE IRA-402BL, and another ion exchange column packed with AMBERLITE IRA-743T is installed downstream.

## DEPR:

Hence it was verified that if the conditions are the same, boron can be reduced to the same level as that of Example 2. That is to say, in Example 3 the boron concentration of the effluent of the ion exchange column 300 was the same as that of Example 2 when the exhaustion cycle was carried out under the same conditions.

## DEPR:

Due to the fact that the ion exchange column 300 packed with Amberlite IRA-743T is a separate column from the A column 331 in Example 2, it is easy to provide an independent regeneration means for the ion exchange column 300. More specifically, the boron selective ion exchange resin can be regenerated to its ideal state (higher boron adsorption capacity) by passing the acidic aqueous solution for regenerating the K column through this column 300 before or after passing it through the K column so as to rapidly elute boron, and then passing the alkaline aqueous solution for the A column 33 through the column 300.

## DEPR:

FIG. 5 shows a part of a high purity water producing apparatus. In this example, the K column 311 of Example 1 is replaced by a K column 31 charged only with a cation exchange resin. Further, the mixed bed ion exchange apparatus (MB column) 8 packed with an anion exchange resin and a cation exchange resin in the conventional high purity water producing apparatus, is replaced by a regenerative type mixed bed ion exchange apparatus 800 wherein a boron selective ion exchange resin is mixed with the anion exchange resin and cation exchange resin.

## DEPR:

Using a high purity water producing apparatus provided with the regenerative type mixed bed ion exchanger 800 shown in FIG. 5, high purity water was produced under the same conditions as those of Example 1 except for the ion exchange resins as described below (the K column 311 of the two bed ion exchange system 3 was packed only with AMBERLITE IR-124), and the boron concentration of the effluent of the exchanger 800 was measured by an ICP-MS analyzer. The results for boron concentration were the same as those of Example 1 shown in FIG. 2.

## DEPR:

As a strongly basic anion exchange resin was used in admixture with a strongly acidic cation exchange resin, ion exchange was effected under the near neutral conditions which permitted the maximum utilization of the capacity of the boron selective resin, this in turn resulted in minimizing the quantity of the boron selective resin.

DEPR:

Manufacture of the ion exchange columns and regeneration means are easy.

DEPR:

By adding a boron selective ion exchange resin to an existing regenerative type mixed bed ion exchanger, or by making simple modifications of an existing regeneration means as necessary, an existing apparatus may be converted to a deionized or high purity water producing apparatus with a function for removing boron.

DEPR:

The example shown in FIG. 6 has the same basic treatment scheme as the conventional high purity water producing apparatus shown in FIG. 17 (where the K column 311 of FIG. 1 is replaced by the K column 31 packed only with an ordinary cation exchange resin), and a non-regenerating ion exchange column 400 packed only with AMBERLITE IRA-743T, which is a boron selective ion exchange resin, is provided between the regenerative type mixed bed ion exchanger 8 and the primary deionized water tank 9. The remaining features of the construction are the same as those of the conventional high purity water producing apparatus.

DEPR:

Apart from the modifications mentioned hereinabove, high purity water was produced continuously for 30 days under the same conditions as those of Example 1, and the boron concentration of the effluent leaving the ion exchange column 400 was measured by an ICP-MS analyzer. The results are shown in FIG. 7.

DEPR:

For purposes of comparison, the non-regenerating ion exchange column 400 packed with AMBERLITE IRA-743T of Example 5 was replaced by a non-regenerating ion exchange column 401 packed with AMBERLITE IRA-402BL, and high purity water was produced under the same conditions as those of Example 5. The boron concentration of the effluent from the column 401 was measured by an ICP-MS analyzer. The results are shown in FIG. 7. In this case, the boron concentration fluctuated, and considerable leakage of boron occurred in 13 days after the start of the exhaustion cycle.

DEPR:

As can be seen from a comparison of Example 5 and Comparative Example 2, boron was effectively removed by the apparatus of Example 5, and thanks to the use of a non-regenerating ion exchange column, there is no variation of water quality due to regeneration.

DEPR:

In the example of FIG. 8, an RO apparatus comprising a reverse osmosis membrane is interposed between the non-regenerative type ion exchange column 400 packed with AMBERLITE IRA-743T and the primary deionized water tank 9 of Example 5 shown in FIG. 6, the remaining features of the treatment scheme being identical to those of Example 5.

DEPR:

In this example, in addition to the advantages of Example 5, organic matter eluted from the boron selective ion exchange resin are removed by the RO membrane 402, so TOC in the secondary deionized water production system is reduced.

DEPR:

This example, which is shown in FIG. 9, has the same basic treatment scheme as the conventional high purity water producing apparatus shown in FIG. 17 (where the K column 311 of FIG. 1 has been replaced by the K column 31 packed only with an ordinary cation exchange resin). A branch pipe 901 downstream of a pump 900 for supplying primary deionized water from the primary deionized water tank 9 to the secondary deionized water treatment system is provided, part of the primary deionized water thereby being supplied to the secondary deionized water system and the remaining primary deionized water being used for other purposes in which existence of boron does not pose any serious problem. A non-regenerative type ion exchange resin column 500 charged with the aforesaid Amberlite IRA-743T, which is a boron selective ion exchange

resin, is provided downstream of this branch 901 at the stage preceding the ultraviolet oxidizer 10 of the secondary deionized water treatment system (upstream). An RO apparatus comprising a reverse osmosis membrane is installed at the stage following the ion exchange column 500 as in the case of the apparatus shown in Example 6

DEPR:

In the apparatus of this example, the same boron removal is achieved as in the case of the aforesaid Example 5, and due to the installation of the ion exchange column 500 downstream of the branch pipe for water for other uses, from which it is not necessary to remove boron, the ionic load on the ion exchange resin is decreased and the amount of resin used can be reduced. As the amount of water used for other purposes is frequently twice the amount of high purity water or more, the arrangement of this example presents a significant advantage.

DEPR:

FIG. 10 shows the partial construction of a high purity water producing apparatus. In this example, instead of the cartridge polisher 11 of the high purity water producing apparatus in Example 17, a boron meter 120 and a pair of cartridge polishers 111a and 111b each packed with a boron selective ion exchange resin and connected in series are provided, and merry-go-round operation is performed by switching valves V1-V12.

DEPR:

In the cartridge polishers 111a and 111b, a boron selective ion exchange resin is charged as the upper layer on a mixed bed of a cation exchange resin and an anion exchange resin.

DEPR:

In this apparatus, the cartridge is replaced when the boron concentration in the effluent of the first cartridge polisher 111a has reached a predetermined concentration. Describing the merry-go-round operation with reference to FIG. 11-FIG. 13, in FIG. 11, the state of the valves is V1 open, V2 closed, V3 open, V4 open, V5 closed, V6 open, V7 open, V8 closed, V9 open, V10 open, V11 closed and V12 open. In this state, primary deionized water supplied from the primary deionized water tank 9 is passed through the ultraviolet oxidizer 10, cartridge polisher 111a, cartridge polisher 111b and the ultrafiltration membrane apparatus 12, as shown by the bold line in FIG. 11. The boron meter 120 is installed between the first cartridge polisher 111a and the second cartridge polisher 111b so that the quality of the treated water from the first polisher 111a can be constantly monitored. When the value measured by the boron meter 120 has reached a predetermined value, it is concluded that the lifetime of the polisher 111a has been reached. The valves are then changed over to the state V1 closed, V2 open, V3 open, V4 closed, V5 open, V6 open, V7 open, V8 closed, V9 closed, V10 closed, V11 closed and V12 closed, the spent cartridge polisher 111a is removed as shown in FIG. 12, and the primary deionized water supplied from the tank 9 is treated only by the polisher 111b as shown by the bold line in FIG. 12. After a new cartridge polisher 111c has been fitted to replace the polisher 111a which was removed as shown in FIG. 13, the valves are changed over and water begins to be passed through the system so that the polisher 111b is the first stage and the new polisher 111c is the second stage. The state of the valves shown in FIG. 13 is V1 closed, V2 open, V3 open, V4 closed, V5 open, V6 open, V7 closed, V8 open, V9 open, V10 closed, V11 open and V12 open. Primary deionized water then flows in the order of ultraviolet oxidizer 10--cartridge polisher 111b--cartridge polisher 111c--ultrafiltration membrane apparatus 12.

DEPR:

FIG. 14 shows the case where an ultraviolet oxidizer 40 is situated between the RO apparatus 5 comprising a reverse osmosis membrane and the vacuum degasser 7 in the high purity water producing apparatus of FIG. 17, ion exchange columns 80a and 80b each containing layers of the boron selective resin and an anion exchange resin are installed in place of the regenerating mixed bed ion exchanger 8, and the treatment scheme includes a boron meter 20 in a so-called merry-go-round arrangement as shown in FIG. 14. In FIG. 14, dissolved TOC in the water treated by the RO apparatus 5 is decomposed into organic acids and carbon dioxide by the ultraviolet oxidizer 40, and then the dissolved oxygen and part of the dissolved carbon dioxide is removed by the

vacuum degasser 7. Next, anions and boron which are present in minute amounts are removed by the layer type (stratified) ion exchange columns 80a and 80b. The columns 80a and 80b are regenerative type ion exchange columns, and after regenerating the first column using auxiliary regenerating means, water treatment begins in the arrangement where the first column is situated at a down stream side of the second column. The treated water from the columns 80a and 80b is sent to the primary deionized water tank 9. The treatment scheme after the ultraviolet oxidizer 10 is the same as that of Example 8, and the cartridge polishers 111a and 111b containing the boron selective resin are installed in a "merry-go-round" system, while a boron meter 120 is situated between the cartridge polishers 111a and 111b. High purity water is supplied to points of use 13 via the ultrafiltration apparatus 12.

DEPU:

3 Two bed ion exchange deionization system

DEPU:

300 Ion exchange column

DEPU:

400 Ion exchange column

DEPU:

500 Ion exchange column

CLPR:

1. A deionized or high purity water producing method comprising: (a) pretreating feed water to remove suspended solids in the feed water, (b) contacting the pretreated water with (i) a first ion exchange resin and (ii) a second ion exchange resin comprising a boron selective ion exchange resin so as to remove boron contained in said pretreated water, and (c) stratifying or mixing together the first and second resins within an ion exchange column.

CLPR:

2. A deionized or high purity water producing apparatus comprising (a) a pretreatment unit comprising means for removing suspended solids in feed water, and (b) a purification treatment section comprising deionization means and membrane separation means for removing ionic and non-ionic substances contained in effluent of said pretreatment unit, wherein:

CLPR:

9. An apparatus as defined in claim 8, wherein at least one of an ultraviolet oxidizer and a reverse osmosis membrane apparatus are provided downstream of said ion exchange column containing said boron selective ion exchange resin.

CLPV:

said deionized or high purity water producing apparatus includes an ion exchange column containing (i) a first ion exchange resin and (ii) a second ion exchange resin comprising a boron selective ion exchange resin, wherein said first and second resins are stratified or mixed together, and said column is provided in at least one location downstream from said pretreatment unit.

CLPV:

said purification treatment section comprises a primary deionized water production system comprising membrane separation means for obtaining a primary deionized water from pretreated water produced by said pretreatment unit, a tank for storing the primary deionized water, and a secondary deionized water production system comprising at least one of ion exchange means, and membrane separation means for obtaining high purity water after said primary deionized water has passed through said tank, said ion exchange column being provided in at least one location in said primary deionized water production system, in said secondary deionized water production system, or between said primary deionized water production system and said secondary deionized water production system.

CLPV:

said boron selective ion exchange resin contained within said ion exchange resin column is capable of being regenerated and further comprising means for regenerating the resin within the column, said regenerating means including

means for passing at least one of the following regenerating agents: an acidic aqueous solution and an aqueous alkaline solution through said ion exchange resin.

CLPV:

said ion exchange resin column is a single column containing a cation exchange resin in the form of a layer downstream of said boron selective ion exchange resin, and said regenerating means comprises means for passing an acidic aqueous solution as a regenerating agent through said column.

CLPV:

said ion exchange resin column is a single column containing an anion exchange resin in the form of a layer upstream of said boron selective ion exchange resin, and said regenerating means comprises means for passing an alkaline aqueous solution as a regenerating agent through said column.

CLPV:

said ion exchange resin column is an ion exchange column containing a mixture of said boron selective ion exchange resin, a cation exchange resin and an anion exchange resin.

CLPV:

said boron selective ion exchange resin contained within said ion exchange resin column is not capable of being regenerated and said ion exchange resin column is provided downstream of said tank for storing primary deionized water; and a branch pipe is provided extending from a point downstream of said primary deionized water storage tank.